

Appl. No. 10/723,738

Amendment dated January 30, 2006

Reply to Office Action of September 30, 2005

**AMENDMENTS TO THE CLAIMS:**

This listing of claims will replace all prior versions, and listings, of claims in the application:

**Listing of Claims:**

1. (currently amended): A process for the treatment of waste gas wherein the waste gas is contacted with a zeolite Y which has a unit cell size of 24.17-24.45 Å and a water adsorption capacity ( $p/p_0 = 0.2$ ,  $T=25^{\circ}\text{C}$ ) of at most 5 wt.%, said zeolite Y having a bulk silica-alumina molar ratio of at least 40.
2. (currently amended): The process of claim 1 wherein the waste gas is engine exhaust gas, ~~in particular exhaust gas from a diesel or gasoline engine.~~
3. (previously presented): The process of claim 1, wherein the zeolite functions as an adsorbent which adsorbs organic hydrocarbons at a low temperature and desorbs them at a higher temperature.
4. (previously presented): The process of claim 1 wherein the zeolite is part of an oxidation catalyst, the zeolite optionally comprising a noble metal of Group VIII of the periodic table of elements.
5. (previously presented): The process of claim 1 wherein the zeolite is part of a  $\text{No}_x$  reducing catalyst and/or of a  $\text{No}_x$  trap catalyst, the zeolite optionally comprising noble metal of Group VIII of the periodic table of elements and/or a non-noble metal of Group VIII of the periodic table and optionally an alkaline earth metal component such as barium.
6. (previously presented): The process of claim 1 wherein the zeolite is periodically subjected to a temperature above  $350^{\circ}\text{C}$ .
7. (withdrawn): A unit suitable for the treatment of exhaust gas according to the process of claim 1, which comprises a zeolite Y which has a unit cell size of 24.17-

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24.45 Å, a water adsorption capacity ( $p/p_0 = 0.2$ ,  $T=25^{\circ}\text{C}$ ) of at most 5 wt.%, and a silica-alumina molar ratio of at least 40.

8. (withdrawn): The unit of claim 7 which comprises a monolith at least part of the surface of which is coated with the zeolite.

9. (withdrawn): The unit of claim 7 which additionally comprises a Group VIII non-noble metal and/or a Group VIII noble metal, and/or an alkaline earth metal, and/or a Group I metal.

10. (currently amended): A process for the treatment of exhaust gas from a diesel engine, wherein the engine exhaust system is provided with a hydrocarbon adsorbent and/or an oxidation catalyst and/or a  $\text{NO}_x$  conversion catalyst and/or a  $\text{NO}_x$  trap catalyst, wherein the hydrocarbon adsorbent and/or the oxidation catalyst and/or the  $\text{NO}_x$  conversion catalyst and/or the  $\text{NO}_x$  trap catalyst comprise a zeolite Y which has a unit cell size of 24.17-24.45 Å, a water adsorption capacity ( $p/p_0 = 0.2$ ,  $T=25^{\circ}\text{C}$ ) of at most 5 wt.% and a bulk silica-alumina molar ratio of at least 40.

11. (previously presented): The process of claim 10 wherein the zeolite is periodically subjected to a temperature above  $350^{\circ}\text{C}$ .

12. (withdrawn): A unit suitable for the treatment of exhaust gas according to the process of claim 10, which comprises a zeolite Y which has a unit cell size of 24.17-24.45 Å, a water adsorption capacity ( $p/p_0 = 0.2$ ,  $T=25^{\circ}\text{C}$ ) of at most 5 wt.% and a silica-alumina molar ratio of at least 40.

13. (withdrawn): The unit of claim 12 which comprises a monolith at least part of the surface of which is coated with the zeolite.

14. (withdrawn): The unit of claim 12 which additionally comprises a Group VIII non-noble metal and/or a Group VIII noble metal, and/or an alkaline earth metal, and/or a Group I metal.